

Comparison of Analysis and Experiment for Self-Acting Seals for Liquid-Oxygen Turbopumps

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### SUMMARY

Two self-acting seal designs (a small and a large) for LOX turbopumps were analyzed in order to predict performance (clearance and leakage). A small (2.86-cm-i.d.) seal to operate at 90 000 rpm and 310 N/cm<sup>2</sup> pressure differential was analyzed for operation from 45 000 to 90 000 rpm (70 to 141 m/sec) and between 103 and 310 N/cm<sup>2</sup> differential. A larger (7.66 cm i.d.) seal to operate at 32 000 rpm and 310 N/cm<sup>2</sup> was analyzed from 24 000 to 36 000 rpm (98 to 147 m/sec) and 172 to 448 N/cm<sup>2</sup>. Three fluid phase cases were studied: fully liquid, fully gas, and intermediate (liquid throughout the pads and gas across the dam).

The analysis predicts that at the design speed and pressure differential, both seals operate at clearances at which no rubbing contact is expected (greater than 0.0025 mm). Test results verify this prediction. The best prediction of trends was obtained by assuming a fully gas state throughout the seal. For this case, predicted leakages were close to one-fourth of experimental for the large seal. Consideration of pertinent factors indicates the fully liquid assumption is invalid for these seals and operating conditions. Evidently the seals operate with mostly liquid in the pads and mostly gas across the dam.

### INTRODUCTION

Turbopump seals in liquid propellant engines must be capable of operation at high speeds and pressures. Leakage rates of sealed fluids (e.g., LOX) must be low despite extreme operating conditions.

Prior technology has depended on rubbing contact seals for minimum leakage rates. Rubbing contact seals have operated successfully for extended periods to  $276 \text{ N/cm}^2$  differential and to 52 m/sec (ref. 1).

But advanced engines will operate at higher pressure differentials and much higher speeds. Two recent applications call for operation to 310 N/cm<sup>2</sup> differential and to 141 and 130 m/sec. This is beyond the entended period capability of rubbing contact seals as indicated in figure 1. Among other problems, the heat generated by rubbing contact at such speed can present an explosion hazard.

One solution is the use of close-clearance hydrodynamic face seals. NASA-designed face seals have performed successfully in tests (ref. 2). These designs are based on computer analyses including the program of reference 3.

The objective of this study is (1) analytically predict seal performance (equilibrium clearance and leakage) and (2) to compare predicted performance with experimental performance. Self-acting radial face seals of two sizes (2.86 and 7.66 cm i.d.) were analyzed. The smaller was studied over the ranges of 45 000 to 90 000 rpm (70 to 141 m/sec) and 103 to 310 N/cm<sup>2</sup> pressure differential. The larger was studied over 24 000 to 36 000 rpm (98 to 147 m/sec) and 172 to 448 N/cm<sup>2</sup> differential. The experimental data was obtained with LOX near the boiling point at the sealed pressure.

### TEST SEALS

The seals studied here were designed and analyzed for performance at Lewis Research Center. Testing of the seals was done - under two contracts - by Rocketdyne Division of Rockwell International.

The SSME LOX turbopump seal system in which the larger of the two seals to be analyzed can be applied is shown in figure 2. Propellant  $(H_2)$  vapor is separated from oxidant  $(O_2)$  by a purge gas (He). The flow directions are indicated. The propellant is vented between two ring seals and also adjacent to a purge gas seal. The oxidant is vented adjacent to the other purge gas seal.

The small seal was intended for application in the space tug engine. A schematic is presented in figure 3. The test rig for this seal is described in reference 2. The configuration of and the test rigs for the two seals are similar.

Both seals are close-clearance hydrodynamic radial face seals with shrouded Rayleigh step bearing lift pads. The sealed fluid is at the outside diameter of both. The seal dams are adjacent to the inside diameter - inside the lift pads. Both are spring loaded and have piston ring secondary seals. From the standpoint of analysis, they are basically identical. The dimensions of interest in analysis are presented in table I. Both seals have a flow length (across the dam) of 0.13 cm; both have 10 lift pads with a recess arc to land arc ratio of 2 to 1.

### OPERATING CONDITIONS ANALYZED

The small seal was designed to operate at speeds up to 90 000 rpm (141 m/sec) and pressure differentials up to 310 N/cm $^2$ . Speeds of 45 000, 60 000, 75 000, and 90 000 rpm and differentials of 103, 172, 241, and 310 N/cm $^2$  were selected as points for analytical study.

The large seal was designed to operate to 32 000 rpm (130 m/sec) and 310  $\rm N/cm^2$  differential. However, overspeed (86 000 rpm) and overpressure (448  $\rm N/cm^2$ ) are in-

cluded in the test schedule. It was studied at four speeds: 24 000, 28 000, 32 000, and 36 000 rpm and five differentials: 172, 241, 310, 379, and 448  $N/cm^2$ .

Due to shear heating and pressure drop, it is probable that some or all of the LOX will evaporate in the pads or while passing across the dam. The limiting fluid conditions will be either liquid throughout the pads and dam or gas throughout. A likely intermediate condition is the assumption of liquid throughout the pads and gas across the dam. Conduction and heat of vaporization absorb shear energy in the pads while vaporization is expected to commence near the entrance of the dam. The required properties were obtained from the tables of reference 4 by linear interpolation. For gas flow across the dam, properties will change appreciably. Mean values of pressure ( $P_{\rm sealed} - 1/3 \Delta P$ ) at the boiling point of the sealed pressure were used. For liquid across the dam and for analysis of the pads, properties at the sealed pressure and its boiling point were used.

### RESULTS AND DISCUSSION

### Analysis

The three cases (conditions) of operation studied were (1) fully liquid assumed, (2) fully gas assumed, and (3) liquid throughout the pads and gas across the dam assumed.

Fully liquid assumed. - Results of analysis are presented in figure 4(a) (small seal) and (b) (large seal). It was assumed that shear heating will vaporize most or all of the LOX at clearances less than about 0.0025 mm; therefore, lower clearances were not evaluated for the fully liquid condition. At the 448-N/cm² differential, the heat of vaporization is low enough that most or all liquid in the seal vaporizes; this differential was not analyzed for the fully liquid case. It can be seen that, at a given pressure differential, clearance - and therefore leakage - increases with speed. And above a speed that depends on the differential, these curves are nearly linear. In the pressure range studied, clearance (and leakage) increases with decreasing differential at constant speed.

Although this discussion is based on figure 4(a) (small seal), enough clearances (above about 0.0025 mm) were analyzed for the large seal to indicate that its behavior is qualitatively the same.

Fully gas assumed. - In figures 5(a) (small seal) and (b) (large seal) only points for which analysis indicates turbulent flow across the dam (the pads analyzed as turbulent to clearances above 0.0025 mm) are presented. As expected, the predicted behavior of both seals is qualitatively the same. Again clearance and leakage increase with speed at constant pressure differential. However, the rate of increase is less than for the fully liquid case.

At constant speed, the effect of density and of pressure differential on the leakage is observed. There is very little change in clearance.

Intermediate (liquid in pads, gas in dam). - Results when turbulent flow across the dam is predicted are presented in figures 6(a) (small seal) and (b) (large seal). Again the  $448 \text{ N/cm}^2$  differential was not analyzed. As with the other two cases, there is an increase of clearance and leakage with speed at constant pressure differential.

However, for constant speed, the leakage reaches a maximum and decreases although clearance continues to increase as differential decreases.

Comparison of conditions. - A comparison of figures 4(a), 5(a), and 6(a) - for the small seal (the large seal is similar) - shows that clearance and leakage increase with increasing speed at constant pressure differential for all three cases although there is a more rapid increase for the fully liquid case. The other two cases (figs. 5(a) and 6(a)) show similar trends at constant differential.

For constant speed, the fully gas case differs from the other two. The fully liquid case curves show decreasing slopes - it can be anticipated that as pressure differential decreases, the leakage rate will eventually begin to decrease.

In table II, results for a selected portion of the ranges studied are presented for direct comparison. In the ranges of speed and pressure differential covered, the intermediate case (3 above) has the greatest clearance. Which condition has the least clearance depends on both speed and differential. As speed increases (at constant pressure differential) or as differential decreases at constant speed, the clearance of the all gas case increases relative to that of the all liquid case and becomes larger than the all liquid. It can also be seen that although the all gas case shows little effect of pressure differential on clearance, the intermediate case shows a decrease in clearance as pressure rises; and the single point at the 379 N/cm<sup>2</sup> differential for the large seal at which comparison is possible shows that the intermediate case no longer has the greatest clearance. In table II, the all liquid case shows the greatest leakage rates. However, consideration of clearance and leakage trends indicates that at low enough speed or high enough pressure differential, the all liquid rate will fall below that of one or both of the order cases. This is actually predicted for the large seal.

At the design speed (small: 141 m/sec; large: 130) and pressure differential (both:  $310 \text{ N/cm}^2$ ), analysis of the small seal indicates clearances of 0.0086 mm for the all liquid case, 0.0089 mm for the all gas condition and 0.015 mm for the intermediate conditions. For the large seal, clearances of less than 0.0025 mm (all liquid), 0.0064 mm (all gas) and 0.0056 mm (intermediate) are predicted at design speed and differential. Since the all liquid case probably does not occur at design operation, it can be assumed that contact will occur only during startup and shutdown. This is confirmed by test reports that generally indicate little or no wear and no surface damage.

### Comparison of Analysis and Experiment

The model used for gas flow across the dam does not consider rotational shear heating and rotationally induced turbulence. The model used for liquid in the pads neglects the presence of the side rails of the pad recesses. One obvious result for both models is prediction of a lower clearance.

In table III, the experimental speeds, pressures, and leakages for several test runs are presented together with the analytical results.

For the small seal test point, the intermediate case analysis offers the best agreement with experiment. The all liquid analysis predicts far too high a leakage while the all gas prediction is too low.

For the large seal test points, the all gas predictions show excellent qualitative agreement being very close to the estimated leakage. However, even the shortcoming of the dam model appears insufficient to account for the difference between analysis and experiment. Obviously at least a large portion of this seal is operating in a fully liquid condition.

The fully liquid and intermediate cases show the shortcoming of the model used for analysis of liquid throughout the pads. As is apparent, the relative error increases as the predicted clearance decreases. From this consideration it appears that this seal is not operating in a fully liquid condition. At the largest predicted clearance (for fully liquid) leakage is about twice the experimental value even though the error is still appreciable (clearance is under half the recess depth).

The largest predicted clearance for the intermediate condition has a leakage rate of half the estimated experimental value. Again (as for the small seal), this condition is the closest approximation to reality of the three.

### CONCLUSIONS

Two LOX turbopump seal designs were analyzed over ranges of pressure differential and speed involved in testing the designs. A comparison of analysis and experiment led to the following conclusions:

- 1. Prediction by analysis that the seals would operate without rubbing contact was confirmed by test results.
- 2. Both seals evidently operated with mostly liquid in the pads and mostly gas across the dam.

3. An excellent prediction of performance trends was obtained by assuming gas throughout the seals. However, the low predicted leakage rates showed this assumption to be incorrect.

Lewis Research Center,
National Aeronautics and Space Administration,
Cleveland, Ohio, January 9, 1979,
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TABLE I. - NOMINAL SEAL FACE DIMENSIONS

	Dimension	Small	Small Large
		seal	seal
Ą	A Pad land arc, radians	0.192	0.196
В	Pad recess arc, radians	0.384	0.392
ပ	Pad outside diameter, cm	4.48	9.40
О	Pad inside diameter, cm	3.36	8.17
Ħ	Pad outer rail inside diameter, cm	4.38	9.29
ᅜ	Pad inner rail outside diameter, cm	3.47	8.28
Ö	Seal dam outside diameter, cm	3.11	7.91
H	Seal dam inside diameter, cm	2.86	7.66
н	Pad recess depth, cm	0.0015	0.0018
-	Balance diameter, cm	2.93	7.73

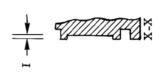
# TABLE II. - VALUES OF CLEARANCE AND LEAKAGE FOR REPRESENTATIVE POINTS OF SMALL SEAL

PERFORMANCE MAP

Assumed state	of fluid			
75 000 rpm	Leak-	age,	kg/min	
75 00	Clear-	ance,	mm	
rpm	Clear- Leak- Clear- Leak-	age,	kg/min	
60~000~rpm	Clear-	ance,	mm	
Pressure	differential, $N/cm^2$			

All liquid	All gas	Intermediate	(pads: liquid;	dam: gas)
2.33	. 15	. 46		
0.0126	.0075	.0193		
1.42	. 12	.34		
0.0091	.0064	.0149		
172				

All liquid All gas Intermediate	All liquid All gas Intermediate
1.68	1.15 .26 .47
0.0092 .0075	0.0067 .0074 .0120
0.90	0.50
0.0062 .0063 .0116	0.0041 .0062 .0089
241	310



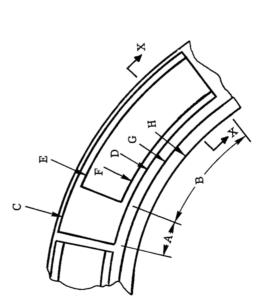
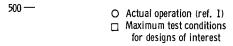


TABLE III. - COMPARISON OF PREDICTED AND MEASURED LEAKAGE

## RATES FOR SELECTED TEST RUNS

Seal	Mean speed of seal dam		Pressur Sealed	e, N/cm <sup>2</sup>	seal	Predicted leakage for assumed states, kg/min		
	rpm/1000 m/sec		beateu	Ambient	leakage, a			
					kg/mm	Liquid	Gas	Interme- diate <sup>b</sup>
Small	75.9	119	269	11. 7	0.37	1.62	0.22	0.45
Large	35.5	145	180	19.0	1.20	2.23	. 30	. 59
Large	32.0	130	223	19.3	1. 43	.80	. 36	. 47
Large	33.6	137	281	22.3	1.83	. 44	. 49	. 49

<sup>&</sup>lt;sup>a</sup>Estimated as one half of total. <sup>b</sup>Pads: liquid; dam: gas.





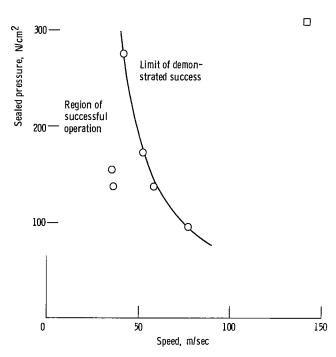


Figure 1. - Required speeds and sealed pressures compared during successful operation for extended periods in sealing of LOX by contact face seals.

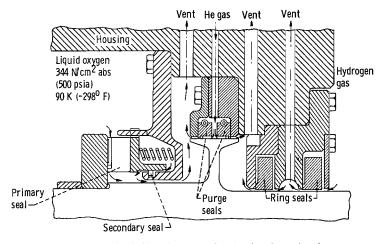


Figure 2. - Schematic of LOX turbopump seal system for advanced engine.

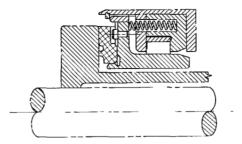


Figure 3. - NASA designed oxygen face seal with composite piston ring for tug vehicle.

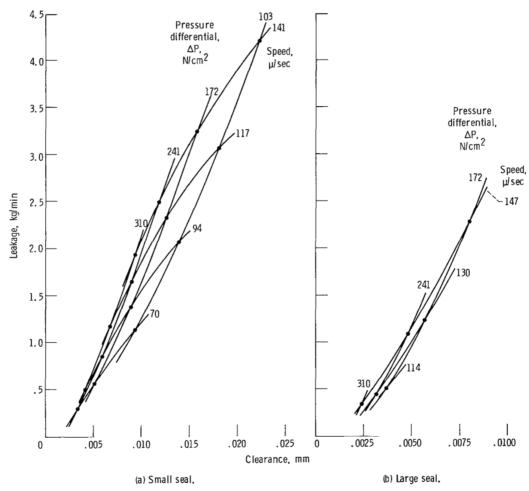


Figure 4. - Sea! performance for fully liquid case. LOX at several speeds and pressure differentials.

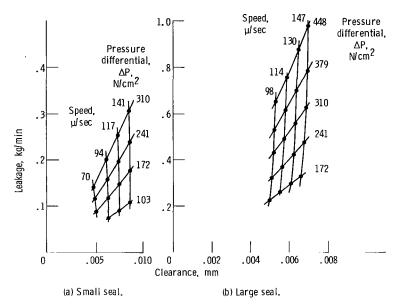


Figure 5. - Seal performance for fully gas case. LOX at several speeds and pressure differentials.

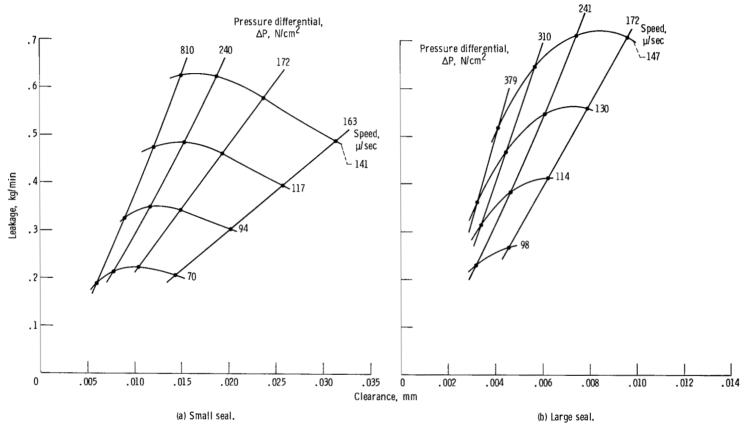


Figure 6. - Seal performance for intermediate (pads: liquid; dam: gas) case. LOX at several speeds and pressure differentials.

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